

GASIFICATION OF LIVESTOCK WASTE WITH ULTRASUPERHEATED MIXTURE OF STEAM AND CARBON DIOXIDE

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Abstract: Experimental studies of steam and CO₂-assisted allothermal gasification of the original (moisture $\alpha = 70\%$) and partly dried pig manure (PM) with $\alpha = 45\%$ and 15% are conducted on a laboratory-scale flow-through gasifier. The high-temperature ($\sim 2000^\circ\text{C}$) gasification agent is generated by a pulsed-detonation gun (PDG) operating on the stoichiometric natural gas–oxygen mixture. The contents of C, O, and H in the dry feedstock are 45.7, 37.7, and 5.8 % (wt.), respectively. The mass fraction of elements with an atomic mass above 11 a.u. in the feedstock is 6.8 % (wt.). The mineral components in the feedstock are mainly represented by compounds of Si, Ca, P, Mg, K, S, Na, Cl, Al, and Fe. The high heating values of the feedstock at $\alpha = 70\%$ and 0% are 5.8 and 16.8 MJ/kg. The dry off-gas obtained from the original feedstock typically contains 33–41 % (vol.) CO₂, 34–40 % (vol.) CO, 17–22 % (vol.) H₂, 2.5–4.0 % (vol.) CH₄, and 0–2.5 % (vol.) C_xH_y with propane being the highest registered hydrocarbon in C_xH_y (less than 0.1%), i.e., there is no tar as a gasification by-product. The reduction of feedstock moisture allows for increasing the yields of CO, H₂, and CH₄ to 45%, 25%, and 5%, respectively, and reducing the yield of CO₂ to 25%. i.e., the resulting dry off-gas can contain up to 75% combustible gas. The mass of fly ash residue is 10%–17% of the dry mass of the original feedstock. With a decrease in the feedstock moisture to $\alpha = 15\%$, the mass of fly ash increases to 20%–30%, i.e., partly dried feedstock is more easily carried away from the flow-through gasifier. Fly ash is found to contain C, O, P, N, K, and H with trace amounts of Si, Ca, Mg, S, Na, Cl, Al, and Fe. The size of fly ash particles ranges from 0.1 to 35 μm . Results of experiments in terms of the off-gas temperature and composition agree satisfactorily with the results of thermodynamic calculations, if one takes heat losses into account. In the existing version of the laboratory-scale setup, only about 33% of the thermal energy of the high-temperature gasification agent is utilized for feedstock gasification, while the rest 67% are transferred to the coolant and environment. At these conditions, gasification of 1 kg of dry feedstock with the use of 1 kg of stoichiometric methane–oxygen mixture results in the production of 1.91 kg of combustible off-gas (diluted with 25–30 % (vol.) CO₂) and 0.09 kg fly ash. To improve the energy efficiency of the gasification process, it is recommended to apply proper thermal insulation and heat recovery. To increase the yield of combustible gas, it is recommended to use the continuous supply of feedstock from a feeder and to improve mixing of feedstock with the gasifying agent. To increase the carbon conversion efficiency, special measures must be taken to prevent premature entrainment of feedstock particles.

Keywords: pig manure; gasification; steam; carbon dioxide; pulsed detonation gun; generator gas; fly ash

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Figure Captions

Figure 1 Photographs of the PM: (a) original feedstock; and (b) and (c) feedstock dried on a hot surface

Figure 2 Infrared spectra of cellulose (a) and of two samples of the original PM: No. 1 (b) and No. 2 (c)

Figure 3 Mass fractions of elements in PM

Figure 4 Schematic of the experimental setup: 1 — mixing and ignition device; 2 — spark plugs; 3 — PDG; 4 — cooling system; 5 — reactor-gasifier; 6 — gas sampling system; 7 — ionization probes; 8 — oxygen and fuel line valves; 9 — reducers; 10 — pressure sensors; 11 — oxygen receiver; 12 — methane (natural gas) receiver; 13 — oxygen source; and 14 — methane (natural gas) source

Figure 5 Reactor-gasifier with hatches at the top and bottom (a) and a splitter pipe for the tangential connection of the PDG (b)

Figure 6 Example of gas and wall temperature records in the upper part of a reactor with two stages of wet feedstock gasification: τ_1 — moisture evaporation stage; and τ_2 — gasification stage. Time zero corresponds to the activation of PDG

Figure 7 Example of records of the flow-through gas analyzer (left scale) and gas and wall temperatures in the upper part of the reactor (right scale) in an experiment with loading a portion of 1 kg wet PM into the reactor

Figure 8 Photograph of the fly ash extracted from a “dry” cyclone

Figure 9 Model of the PM gasification process

Figure 10 Compositions of the dry off-gas produced from the original PM with a moisture of 70% at various gasification conditions; the numbers above the columns are the numbers of the experiments in Table 11

Figure 11 Measured dependencies of CO, H₂, CH₄, and C_xH_y volume fractions on the volume fraction of CO₂ in the dry off-gas produced by gasification of wet PM ($\alpha = 70\%$) and wet coffee grounds ($\alpha = 80\%$) (a) and dried PM ($\alpha = 15\%$) and sawdust ($\alpha = 15\%$) (b)

Figure 12 Measured dependencies of CO, H₂, CH₄, and C_xH_y volume fractions on the volume fraction of CO₂ in the dry off-gas produced by gasification of PM of different moisture (70% to 15%, see Table 11) under different conditions of feedstock loading: batch loading (1) and continuous feed (2) into the reactor

Figure 13 Mass fractions of elements in dried PM (1), fly ash extracted from the “dry” cyclone (2), and fly ash extracted from the “wet” cyclone (after drying, 3)

Figure 14 Oxidative stability of fly ash measured by synchronous thermal analysis: (a) sample 1; and (b) sample 2

Figure 15 Particle size distribution in fly ash: 1 — experiments No. 3 + No. 6 in Table 11; 2 — experiment No. 3; 3 — experiment No. 6; 4 — experiment No. 7; 5 — experiment No. 9; and 6 — experiment No. 10

Figure 16 Total ion current chromatograms of diethyl ether (a) and hexane (b) extracts of trimethylsilyl derivatives of condensed products of PM gasification

Table Captions

Table 1 Results of elemental CHNS analysis of the original PM

Table 2 Results of calorimetric measurements of the higher heating value of the original PM

Table 3 Dependence of the mass of the PM sample on the drying time at room temperature

Table 4 Results of calorimetric measurements of the higher heating value of dried PM

Table 5 Elemental composition of dry coffee grounds [47]

Table 6 Elemental composition of wood sawdust [48]

Table 7 Measured composition of detonation products of a stoichiometric methane–oxygen mixture expanded to an initial pressure of 0.1 MPa and a temperature of 2000 K [51]

Table 8 Average statistical composition of PM [52]

Table 9 Model composition of the PM

Table 10 Calculated compositions of the off-gas produced by PM gasification at process temperatures of 1000, 1200, 1500, and 2000 K at a pressure of 0.1 MPa

Table 11 Summary table for conducted experiments

Table 12 Mass balances of PM drying and gasification processes

Table 13 Compositions of the dry off-gas produced by gasification of PM measured in several experiments with a flow gas analyzer and gas chromatographs (marked with an asterisk)

Table 14 Elemental composition of fly ash (%(wt.))

Table 15 Comparison of calculated (equilibrium) and measured compositions of the dry off-gas produced by gasification of PM at a process temperature of 1000 K and pressure of 0.1 MPa

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