

CONVERSION OF RICH PREHEATED METHANE–OXYGEN MIXTURES IN A FLAT STABILIZED LAMINAR FLAME

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Abstract: The article presents the results of kinetic modeling of the process of conversion of rich preheated methane–oxygen mixtures into syngas in the flat stabilized laminar flame in the range of initial temperatures of 300–800 K, fuel-to-air equivalence ratio of 2.4–3.2, and at pressure of 1.5 atm. At the initial temperature of 800 K, the optimal value of the fuel-to-air equivalence ratio $\varphi = 2.77$ (air-to-fuel equivalence ratio $\alpha = 0.361$) is determined, at which the maximum conversion of methane into hydrogen of 79.9% is achieved and the conversion into carbon monoxide is close to the maximum and equals 93.5%. Moreover, with an almost complete conversion of methane of 99.3%, its conversion into carbon dioxide CO₂ is only 5.0% and into water — 19.6%. These results virtually coincide with the experimental results of matrix conversion of methane–oxygen mixtures into syngas, in which similar preliminary heating of the gas mixture to approximately the same temperature occurs due to internal heat recovery of hot syngas. The obtained results indicate the adequacy of the presented kinetic modeling of the processes of gas-phase oxidative conversion of methane into syngas.

Keywords: methane; oxygen; hydrogen; syngas; oxidation conversion; kinetic modeling

DOI: 10.30826/CE25180102

EDN: XPXJSO

Figure Captions

Figure 1 Profiles of temperature (*a*), velocity of the reacting mixture (*b*), and concentrations of reagents (*c*) and main products (*d*) of a stabilized flat laminar flame of a methane–oxygen mixture. Fuel-to-air equivalence ratio is 2.77, pressure is 1.5 atm, and initial temperature is 800 K. Signs — calculation results; curves — corresponding splines; and *x* — coordinate directed along the gas flow: *x* = 0 — burner inlet and *x* = 10 cm — burner outlet

Figure 2 Dependences of conversions of methane to hydrogen on the fuel-to-air equivalence ratio at pressure of 1.5 atm and initial gas temperatures of 300 (*1*), 600 (*2*), 700 (*3*), and 800 K (*4*): signs — calculation results; and curves — corresponding splines

Figure 3 Dependences of total methane conversion (*1*) and of conversions of methane into hydrogen (*2*), water (*3*), CO (*4*), and CO₂ (*5*) on the fuel-to-air equivalence ratio at pressure of 1.5 atm and initial gas temperature of 800 K: signs — calculation results; and curves — corresponding splines

Table Captions

Table 1 Initial flow rates of unburned gas which are set at the burner inlet

Table 2 Key reactions controlling the process of conversion of rich methane–oxygen mixtures at pressure of 1.5 atm and initial temperature of 800 K in the vicinity of the maximum of the derivative of the mole fraction of the hydroxyl radical with respect to the coordinate *x*

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Received December 23, 2024

After revision January 9, 2025

Accepted January 16, 2025

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